

## M3A10: §1.2 Dynamics and the stress tensor

The forces that act on a fluid element are of two kinds:

(i) Volume or body forces, having long range, that are proportional to the *volume* of a fluid element (e.g. gravity).

(ii) Surface tractions, having short range, that are proportional to the *surface area* of a fluid element. Let  $\mathbf{n} dS$  be an arbitrary element of area drawn in the fluid at  $(\mathbf{x}, t)$ . We write the force exerted *by* the fluid on the +side of  $dS$  on the fluid on the –side as  $\boldsymbol{\tau} dS$ .  $\boldsymbol{\tau}$  is called the *surface traction* and depends not only on  $\mathbf{x}$  and  $t$ , but also upon  $\mathbf{n}$ . We define the **Cauchy stress tensor**  $\sigma_{ij}(\mathbf{x}, t)$  such that  $\sigma_{i1}$  is the force acting on a small surface element whose normal points in the 1-direction, and similarly for  $\sigma_{i2}$  and  $\sigma_{i3}$ .

### Theorem 1: Tractions and Stress

We claim that for a general surface element with normal  $\mathbf{n}$ ,

$$\tau_i = \sigma_{ij} n_j .$$

*Proof.* Let  $V(t)$  be an arbitrary material volume of fluid having surface  $S(t)$ . The momentum of the fluid in  $V(t)$  is then

$$\int_{V(t)} \rho \mathbf{u} dV.$$

Thus the equation of motion for the fluid in  $V(t)$  is

$$\frac{d}{dt} \int_{V(t)} \rho \mathbf{u} dV = \int_{V(t)} \mathbf{F} dV + \int_{S(t)} \boldsymbol{\tau} dS . \quad (1.12)$$

Now suppose that  $V$  is small, having linear dimension  $\varepsilon$ . Then because volume integrals have size  $O(\varepsilon^3)$ , whereas surface integrals are  $O(\varepsilon^2)$ , then in the limit  $\varepsilon \rightarrow 0$  the surface terms in equation (1.12) must balance at leading order, and so

$$\lim_{\varepsilon \rightarrow 0} \int_{S(t)} \boldsymbol{\tau} dS = 0.$$

Now take  $V$  to be instantaneously a small tetrahedron as sketched, with a sloping face having area  $dS$  and normal  $\mathbf{n}$ . The other faces have areas

$$n_1 dS, \quad n_2 dS, \quad n_3 dS$$

Because the surface forces on this tetrahedron must balance,

$$\tau_i dS + \sigma_{i1}(-n_1)dS + \sigma_{i2}(-n_2)dS + \sigma_{i3}(-n_3)dS = 0.$$

Hence, as required,

$$\tau_i = \sigma_{ij}n_j . \quad (1.13)$$

## Theorem 2: Symmetry of the stress tensor

Provided no ‘body couples’ act on the fluid,

$$\sigma_{ij} = \sigma_{ji}. \quad (1.14)$$

*Proof.* Taking the origin to lie instantaneously within  $V(t)$ , the angular momentum of fluid in  $V$  is

$$\int_{V(t)} \rho \mathbf{x} \wedge \mathbf{u} dV,$$

and this has magnitude  $O(\varepsilon^4)$ . Now conservation of angular momentum implies that (in the absence of any ‘body couples’ e.g. a ferrofluid in a magnetic field)

$$\frac{d}{dt} \int_{V(t)} \rho \mathbf{x} \wedge \mathbf{u} dV = \int_{V(t)} \mathbf{x} \wedge \mathbf{F} dV + \int_{S(t)} \mathbf{x} \wedge \boldsymbol{\tau} dS . \quad (1.15)$$

The last term here has magnitude  $O(\varepsilon^3)$ , and is therefore larger than the other two terms. Thus at leading order it must vanish, i.e.

$$\lim_{\varepsilon \rightarrow 0} \int_{S(t)} \mathbf{x} \wedge \boldsymbol{\tau} dS = 0.$$

Using theorem 1, the  $i^{\text{th}}$  component of this equation may be written

$$\begin{aligned} \int_S \varepsilon_{ijk} x_j \sigma_{km} n_m dS &= \int_V \varepsilon_{ijk} \frac{\partial}{\partial x_m} (x_j \sigma_{km}) dV \\ &= \int_V \varepsilon_{ijk} x_j \frac{\partial \sigma_{km}}{\partial x_m} dV + \int_V \varepsilon_{ijk} \sigma_{kj} dV. \end{aligned}$$

The integrals here have magnitude  $O(\varepsilon^4)$ , and  $O(\varepsilon^3)$  respectively, so, in the limit  $\varepsilon \rightarrow 0$ ,

$$\varepsilon_{ijk} \sigma_{kj} = 0 \quad \implies \quad \varepsilon_{ilm} \varepsilon_{ijk} \sigma_{kj} = 0 \quad \implies \quad \sigma_{ml} - \sigma_{lm} = 0$$

and thus the stress tensor is symmetric. Alternatively, we can balance the moments of the surface tractions on a cube of side  $\varepsilon$ , as in lectures.

## Equation of motion for a Newtonian fluid

Assuming the fluid is **homogeneous and at rest**, it can have no preferred direction. Now a general stress tensor,  $\sigma_{ij}$  will in general have three eigenvectors, or special directions. It follows that when the fluid is at rest, the stress tensor can be written

$$\sigma_{ij} = -p\delta_{ij} \quad \text{where we shall call } p(\mathbf{x}, t) \quad \text{the pressure.}$$

When motion does occur, we shall write

$$\sigma_{ij} = -p\delta_{ij} + \sigma'_{ij} \quad \text{where } p = -\frac{1}{3}\sigma_{ii} . \quad (1.16)$$

$\sigma'_{ij}$  is called the **deviatoric stress**. In the **inviscid fluid mechanics** course M3A2, it is assumed that  $\sigma'_{ij} \equiv 0$ . More generally, we will assume a linear relationship between the deviatoric stress  $\sigma'_{ij}$  and the velocity gradient tensor  $\partial u_i / \partial x_j$ . This assumption, which is like Hooke's Law for springs, is what defines a **Newtonian fluid**. The linearity relation between the two second-order tensors takes the form

$$\sigma'_{ij} = A_{ijkl} \frac{\partial u_k}{\partial x_l} , \quad (1.17)$$

where  $A_{ijkl}$  is a 4th order tensor, which at first glance contains 81 unknown constant coefficients! However, remember that the fluid is **isotropic** and has no preferred direction. This means that the tensor  $A_{ijkl}$  must be **invariant** with respect to rotations of the coordinate axes. It turns out (see, for example, 'Cartesian Tensors' by Jeffreys) that this requires

$$A_{ijkl} = \lambda\delta_{ij}\delta_{kl} + \mu\delta_{ik}\delta_{jl} + \mu'\delta_{il}\delta_{jk}$$

and so

$$\sigma'_{ij} = \lambda\delta_{ij} \frac{\partial u_k}{\partial x_k} + \mu \frac{\partial u_i}{\partial x_j} + \mu' \frac{\partial u_j}{\partial x_i} .$$

where  $\lambda$ ,  $\mu$  and  $\mu'$  are unknown constants. Furthermore, two of these can be eliminated. Firstly, as we are dealing with incompressible fluids,  $\nabla \cdot \mathbf{u} = 0$  and  $\lambda$  is irrelevant. Secondly, we showed above that  $\sigma_{ij} = \sigma_{ji}$ . This means that  $\mu' = \mu$ . We deduce that the stress tensor  $\sigma_{ij}$  for a Newtonian fluid is

$$\sigma_{ij} = -p\delta_{ij} + 2\mu e_{ij} \quad \text{where } e_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) . \quad (1.18)$$

The constant  $\mu$  is known as the **viscosity** of the fluid.

## The momentum equation for a viscous fluid

With the expression (1.13) for the surface traction  $\boldsymbol{\tau}$ , the equation of motion (1.12) for  $V(t)$  becomes

$$\frac{d}{dt} \int_{V(t)} \rho u_i dV = \int_{V(t)} F_i dV + \int_{S(t)} \sigma_{ij} n_j dS.$$

Using Reynolds' transport theorem (1.3), mass conservation (1.4) and the divergence theorem (0.8) then gives

$$\int_{V(t)} \rho \frac{Du_i}{Dt} dV = \int_{V(t)} F_i dV + \int_{V(t)} \frac{\partial \sigma_{ij}}{\partial x_j} dV.$$

and because  $V$  is arbitrary,

$$\rho \frac{Du_i}{Dt} = F_i + \frac{\partial \sigma_{ij}}{\partial x_j}. \quad (1.19)$$

This is the Cauchy momentum equation for the fluid, and holds for any stress tensor. Now for the Newtonian stress relation (1.18), we have

$$\frac{\partial \sigma_{ij}}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \mu \frac{\partial^2 u_i}{\partial x_j \partial x_j} + \mu \frac{\partial}{\partial x_i} \frac{\partial u_j}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \mu \nabla^2 u_i$$

and so, from (1.19), the momentum equation for a Newtonian Fluid is

$$\rho \frac{D\mathbf{u}}{Dt} = -\nabla p + \mathbf{F} + \mu \nabla^2 \mathbf{u}.$$

We can now, finally, write down the **Navier-Stokes equations**, which we will solve for the remainder of this course. For constant density  $\rho$  and viscosity  $\mu$ , and external force  $\mathbf{F}$ , we have

<h3>The Navier-Stokes Equations for an incompressible fluid</h3>
$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} \right) = -\nabla p + \mathbf{F} + \mu \nabla^2 \mathbf{u}. \quad (1.20)$
$\nabla \cdot \mathbf{u} = 0. \quad (1.21)$

When  $\mu = 0$  we obtain the **Euler equations**, which are the basis of M3A2. Note, however, that as  $\mu \rightarrow 0$ , the fluid does not necessarily behave in the same way as it would if  $\mu = 0$ .